

Systems Study for Improving Gas Turbine Performance for Coal/IGCC Application

Topical Report

Tasks 1-5

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ABSTRACT

This study identifies vital gas turbine (GT) parameters and quantifies their influence in meeting the DOE Turbine Program overall Integrated Gasification Combined Cycle (IGCC) plant goals of 50% net HHV efficiency, \$1000/kW capital cost, and low emissions. The project analytically evaluates GE advanced F class air cooled technology level gas turbine conceptual cycle designs and determines their influence on IGCC plant level performance. This report summarizes the work accomplished in each of the following five Tasks.

- <u>Task 1.0 Overall IGCC Plant Level Requirements Identification:</u> Plant level requirements were identified, and compared with DOE's IGCC Goal of achieving 50% Net HHV Efficiency and \$1000/KW by the Year 2008, through use of a Six Sigma Quality Functional Deployment (QFD) Tool. This analysis resulted in 7 GT System Level Parameters being selected as the most significant for further analysis of IGCC system Requirements at the power island level.
- <u>Task 2.0 Requirements Prioritization/Flow-Down to GT Subsystem Level:</u> GT requirements were identified, analyzed and prioritized relative to achieving plant level goals, and compared with the flow down of power island goals through use of a Six Sigma QFD Tool. This analysis resulted in 11 GT Cycle Design Parameters being selected as the most significant for analysis of Baseline and other IGCC system configurations.
- <u>Task 3.0 IGCC Conceptual System Analysis:</u> A Baseline IGCC Plant configuration was chosen, and an IGCC simulation analysis model was constructed, validated against published performance data and then optimized by including air extraction heat recovery and GE steam turbine model with appropriate last stage buckets. Baseline IGCC based on GE 207FA+e gas turbine combined cycle has net HHV efficiency of 40.5% and net output nominally of 526 Megawatts at NOx emission level of 15 ppmvd@15% corrected O2. 18 advanced F technology GT cycle design options were developed to provide performance targets with increased output and/or efficiency with low NOx emissions.
- <u>Task 4.0 Gas Turbine Cycle Options vs Requirements Evaluation</u>: Influence coefficients on 4 key IGCC plant level parameters (IGCC Net Efficiency, IGCC Net Output, GT Output, NOx Emissions) of 11 GT identified cycle parameters were determined. Results indicate that IGCC net efficiency HHV gains up to 2.8 pts (40.5% to 43.3%) and IGCC net output gains up to 35 % are possible due to improvements in GT technology alone with single digit NOx emission levels.
- <u>Task 5.0 Recommendations for GT Technical Improvements:</u> A trade off analysis was conducted utilizing the performance results of 18 gas turbine (GT) conceptual designs, and three most promising GT candidates are recommended on the basis of their merit on IGCC Efficiency, IGCC Net Output, GT Specific Output and NOx Emissions. For near term (2006): the recommended GT cycle design should have a 2400F class firing temperature, base class compressor pressure ratio (CPR), diffusion combustor and integrated air extraction; for midterm (2008): a 2500F class firing temperature, base class CPR, diffusion combustor, and integrated air extraction; and for long term (2010): a 2600F class firing temperature, increased CPR, and further combustion and hot gas path technology enhancements. A roadmap for turbine technology development is proposed for future coal based IGCC power plants.

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Introduction

Systems Study for Improving GT Performance for Coal/IGCC Applications

A. Objective:

This study identifies impact of gas turbine performance improvements on coal Integrated Gasification Combined Cycle (IGCC) plants and quantifies influence of vital gas turbine parameters in meeting the DOE Turbine Program overall IGCC plant goals of 50% net HHV efficiency, \$1000/kW capital cost, and low emissions. Focus is on air-cooled gas turbines for near-term, year 2008 operation in coal fed oxygen blown IGCC power plants with commercially demonstrated gasification, gas cleaning, & air separation technologies. Gas Turbine conceptual design recommendation plan towards achieving DOE's goals for the Turbine Program is defined, and provides a total systems-level perspective to identify the development needs and improvements that have the highest impact/ payback to the program.

B. Background/Relevancy

Background:

In the near term as reliance on natural gas increases and prices escalate opportunities will arise to reinvest in the use of coal, our nations most abundant fossil fuel resource. Estimates suggest that more than 30 Gigawatts of new coal-based power generation will be installed over the next 15 years. The US generates approximately 50% of its power from coal. Much of this added capacity could be based on integrated gasification combined-cycle technology (IGCC). Significant improvements in overall cycle efficiency and cost per unit of power will dramatically reduce generation costs and emissions. This will help provide low-cost, environmentally acceptable power from a domestically abundant low cost fuel.

Relevancy:

Clean, efficient and cost effective coal based power systems depend on advanced power turbine technology to achieve higher levels of efficiency. IGCC technology has been demonstrated to show superiority in both performance and emissions compared with conventional coal power generation technology. However, additional enhancements in IGCC will be needed to gain superiority in life cycle electricity costs. One area of improvement is in the gas turbine portion of the cycle, which is the primary energy conversion device within an IGCC power plant. Increases in gas turbine conversion efficiency of coal derived syngas energy to power and higher utilization of exhaust energy will help drive lower IGCC plant level generating costs.

Meeting of DOE overall IGCC plant goals of 50% net HHV efficiency, \$1000/kW capital cost, and low emissions for a 500 MW coal plant could provide annual generating cost savings of about \$50 MM/yr compared to current F-Class IGCC systems and about \$20 MM/yr compared to conventional PC technology. Additional enhancements in the area of emitted NOx and SOx could also be realized by making IGCC the technology of choice for coal based power production.

Executive Summary

Overall DOE Turbine Program plant level goals were established from DOE Vision 21 and IGCC Power Plant CURC Roadmap Studies. Using GE's Six Sigma Methodology, key gas turbine (GT) plant level requirements were identified. These gas turbine plant level requirements were used to quantify and prioritize gas turbine cycle parameters. A Baseline Conceptual IGCC System Design was established utilizing current General Electric (GE) F-class gas turbine technology based on a Midwest US IGCC site. An overall IGCC System Performance Model was constructed utilizing GE in- house proprietary software for the gas turbine & steam turbine, and commercially available software for the balance of the systems. The model was exercised through parametric analysis to quantify gas turbine performance impact at IGCC plant system level. Various advanced F class technology gas turbine cycle design options were evaluated to determine performance impact on IGCC efficiency, cost and emissions. Results from the system analysis were used to identify gas turbine technology improvements for development consideration in future Turbine Program phases.

The program includes the following five major tasks, which utilizes GE's Design for Six Sigma methodology:

Task 1 - Overall IGCC Plant Level Requirements Identification:

This task established ranking of DOE's overall IGCC plant level goals of achieving 50% net HHV efficiency and \$1000/kW in year 2008, and is used to prioritize plant level requirements. Using Six Sigma QFD tools, the key IGCC Plant Level parameters identified were: IGCC Net Efficiency, IGCC Net Output, GT Output and NOx Emissions. A subsequent QFD flow down to the most significant GT Plant Level requirements identified the following parameters: Availability, Product Cost, Efficiency, Air Integration flexibility, syngas & diluent supply conditions and syngas NO_x Capability.

Task 2 - Requirements Prioritization & Flow-Down to Gas Turbine Subsystem Level

This task prioritizes GT cycle design parameters from an IGCC Plant Level flow down of GT Plant Level requirements to the GT subsystem level. The most significant GT cycle design parameters were identified as Firing Temperature, Combustor Options, Turbine and Compressor Efficiency, Compressor Pressure Ratio, Cooling Flows, amount of Air Extraction, Syngas Supply Temperature, Diluent Supply Temperature, Compressor Air Flow and Diluent Flow.

Task 3 - IGCC Conceptual System Analysis

A coal-based Baseline IGCC Configuration with Oxygen Blown Gasification and GE F-Class GT technology was defined and then used to validate a Baseline Case IGCC System Performance Simulation Analysis Model. The Simulation Analysis Model was reconfigured to be more consistent with a typical advanced IGCC powerplant by eliminating cogeneration of steam, adding heat recovery from GT air extraction, and using a GE steam turbine with appropriate last stage buckets.

Using this revised IGCC System Performance Simulation Analysis model, eighteen new advanced F technology GT cycle options were analyzed to explore varying turbine configuration impacts that would provide performance targets with increased output and/or efficiency and low NOx emissions. These GT cycle design options were developed by varying the selected system parameters such as Air Integration Method, ASU type, Diluent Method, and Fuel Temperature, as well as GT parameters such as Combustor Type, available Hot Gas Path Configuration including future hardware components, Firing Temperature and Target NOx Level. By modifying the GT subsystem model to create new design options in the integrated IGCC model, performance effects of possible GT technical improvements on key IGCC plant level parameters were analyzed and used to select appropriate GT cycle designs.

Task 4 - Gas Turbine Cycle Options vs. Requirements Evaluation

In this task, IGCC performance derivatives in terms of IGCC Net Plant Efficiency, IGCC Net Plant Output, GT Output and NOx Emissions were evaluated for 11 key GT cycle parameters. The following GT parameters were found to have the greatest impact on each respective plant level derivative: GT Firing Temperature, Turbine & Compressor Efficiency, Diluent Supply Temperature, Compressor Pressure Ratio and Cooling Flows on IGCC Net Efficiency; Firing Temperature, Compressor Inlet Air Flow, Turbine & Compressor Efficiency, Compressor Pressure Ratio and Dilution Flow on IGCC Net Output; Firing Temperature, Compressor Inlet Air Flow, Turbine & Compressor Efficiency and Dilution Flow on GT Output; and Combustion Technology (Diffusion or Premix), Diluent Flow, Firing Temperature and Compressor Pressure Ratio on NOx Emissions.

Using these plant level derivative effects, GT cycle design trade-off studies utilizing the IGCC System Performance Simulation Model and Eighteen new gas turbine cycle options based on advanced F GT technology were analyzed. Results indicate that IGCC efficiency gains up to 2.8 pts (from 40.5% to 43.3%) and IGCC net output gains up to 35 % are possible while still maintaining single digit NOx emission levels with improvements in gas turbine technology alone.

Task 5 - Recommendations for Gas Turbine Technical Improvements

Various GT cycle designs were examined utilizing the performance results to select the most promising candidate cycle concepts. The 3 most promising GT candidates are recommended on the basis of their merit on IGCC Efficiency, IGCC Net Output, GT Specific Output and NOx Emissions. For near term (2006): the recommended GT cycle design should have a 2400F class firing temperature, base class compressor pressure ratio (CPR), diffusion combustor and integrated air extraction; for midterm (2008): a 2500F class firing temperature, base class CPR, diffusion combustor, and integrated air extraction; and for long term (2010): a 2600F class firing temperature, increased CPR, and further combustion and hot gas path technology enhancements. A turbine technology development roadmap is recommended for future coal based IGCC power plants.

Experimental

Overview: Both commercially available software and GE in-house proprietary software

packages were utilized in the analysis phases of this study. A brief description of

their functionality is provided below.

Task 1 - Overall IGCC Plant Level Requirements Identification:

Plant level IGCC requirements were identified, and compared with DOE's IGCC Goals of achieving 50% Net HHV Efficiency and \$1000/KW by the Year 2008, through use of a Six Sigma Quality Functional Deployment (QFD) Tool. This GE in-house, Excel-based, proprietary tool provides a ranking of the importance of IGCC requirements relative to DOE's IGCC Goals.

Task 2 – Requirements Prioritization & Flow-Down to Gas Turbine Subsystem Level

Gas turbine cycle design requirements were identified, analyzed and prioritized relative to achieving plant level goals, and compared with the flow down of power island goals through use of a Six Sigma Quality Functional Deployment (QFD) Tool. This GE in-house, Excel-based, proprietary tool provides a ranking of the importance of gas turbine requirements relative to power island goals.

Task 3 – IGCC Conceptual System Analysis

Overall integrated IGCC system performance model was constructed utilizing GE in-house proprietary software, GateCycleTM for the gas turbine & steam turbine, and commercially available HYSYS Process Modeling software for the balance of the systems. The model is exercised by a parametric analysis in commercial ModelCenter software to quantify gas turbine performance impact at the IGCC plant system level.

Task 4 – Gas Turbine Cycle Options vs. Requirements Evaluation

This integrated IGCC system analysis model is used to determine the influence coefficients of vital Gas Turbine parameters (firing temperature, turbine and compressor efficiency, compressor pressure ratio, diluent and fuel temperature, etc.) on plant-level goals (efficiency, output, emissions, etc). This model is also used for IGCC performance evaluation of various advanced F technology gas turbine cycle design options.

Task 5 – Recommendations for Gas Turbine Technical Improvements

This task did not utilize software tools over and above those used in previous tasks.

Results and Discussion

Task 1 Results/Discussion:

Overview: Gas turbine System level (power island) requirements were identified, and compared with DOE's IGCC Goal of achieving 50% Net HHV Efficiency and \$1000/KW by the Year 2008, through use of a Six Sigma Quality Functional Deployment (QFD) Tool.

Task 1 Discussion:

IGCC Plant Requirements for this study have been based on the DOE Vision 21 Performance Goal for 2008 which outlines a coal-based power system with:

- 1) System HHV based Efficiency of 50%
- 2) Capital Cost of less than \$1000./KW
- 3) NO_x Reduction to less than 2 ppm
- 4) Increase of Heat Engine Efficiency of 2 to 3%
- 5) Attainment of reliability/availability standards for pre-1999 gas turbines

These Plant Requirements are consistent with the CURC/EPRI/DOE Consensus Roadmap as shown below in table 1:

Table 1 - CURC/EPRI/DOE Consensus Roadmap for IGCC Plant Requirements

Item	Reference Plant	2010	2020
Plant Efficiency (HHV)	40%	45-50%	50-60%
Availability	> 80%	> 85%	> 90%
Plant Capital Cost (\$/KW)	1000 - 1300	900 - 1000	800 - 900
Cost of Electricity (cents/KWh)	3.5	3.0 - 3.2	< 3.0
Air Emissions	98% SO ₂ Removal	99% SO ₂ Removal	> 99% SO ₂ Removal
	0.15 lb/10 ⁶ Btu NO _x	0.05 lb/10 ⁶ Btu NO _x	< 0.01 lb/10 ⁶ Btu NO _x
	0.01 lb/10 ⁶ Btu Pariculate	0.005 lb/10 ⁶ Btu Pariculate	0.002 lb/10 ⁶ Btu Pariculate
	Mercury Removal	90%	95%
By-Product Utilization	30%	50%	Near 100%

An analysis of DOE and customer requirements and expectations result in the following set of Power Plant Level Expectations (with corresponding levels of Importance, 5 being the highest):

Power Plant Level Expectations, (Y's)	Importance	Notes:
Low Capital Cost (<\$1000/KW)	5	\$900 – 1000/KW by 2010
High Net Electrical Efficiency (50% HHV)	5	Not Co-Gen or CO ₂ Capture Value
High Availability	5	85% by 2010 through RAM Excellence
Low COE	3	3.2 cents/KWH by 2010
Low Emissions for NO _x and SO _x	3	2 PPM NOx, 99% Sulfur Removal
Fuel Flexibility	3	Low to High Rank Coals, Petcoke
Co-Production Capable	3	Chemical Co-Production, Hydrogen
CO ₂ Removal	3	85% CO ₂ Removal
Reduced H ₂ O Use	2	Driven by Permitting Requirements
Zero Process Discharge	2	Driven by Permitting Requirements

A corresponding set of Gas Turbine Power Island Level Requirements were established as input to the Quality Functional Deployment analysis:

Gas Turbine Power Island Requirements, (X's)

Product Cost (\$/KW)
Generator Output
Efficiency
Availability
Syngas NO_x
Syngas CO
Syngas Fuel Flexibility
Syngas and Diluent Supply Conditions
Diluent Flexibility
Exhaust Gas Energy
Air Integration Flexibility

Notes:

Target of \$200/KW
Maximize
Drives Overall IGCC Efficiency
At Least 95%
9 ppm Ceiling by 2010
9 ppm Ceiling by 2010
Variable CO, H2 Composition
Efficiency, Combustor Requirements
For NO_x Removal
Effect Bottoming Cycle Efficiency
With Air Separation Unit

These Expectations and Plant Requirements are mapped in Figure 1 through the QFD tool, with the weighting factors for the expectations, and the Y's are analyzed against the X's through Low (L), Medium (M) and High (H) levels of connection, with the following results matrix:

IGCC Systems Study QFD

Gas Turbine Power Island Requireme Syngas and Dilluent Supply Condition Air Integration Flexibility Syngas Fuel Flexibility **Expectation** Product Cost \$/KW) Exhaust Gas Energy **Senerator Output** Diluent Flexibility mportance Availability H M High Availability 5 М М 100 High Net Electrical Efficiency - 50% HHV Н М Н М М М Low Capital Cost \$1000/KW M H L M М 5 Н LL CO2 Removal 3 L М M 27 Coproduction Capable 3 М М Fuel Flexibility 3 М L М L Н Н Low COE 3 M M M M Low Emissions Max 0.02 lb/MMBTU NOx and S L 3 Н L L H M M 93 Reduced H2O Use 2 M L M 18 Zero Process Discharge 2 93 92 89 88 84 72 70 52 50 41 14 Total

Figure 1 – Matrix for Plant Level QFD

An alternate representation of the results of the QFD process is the Pareto Chart in Figure 2:

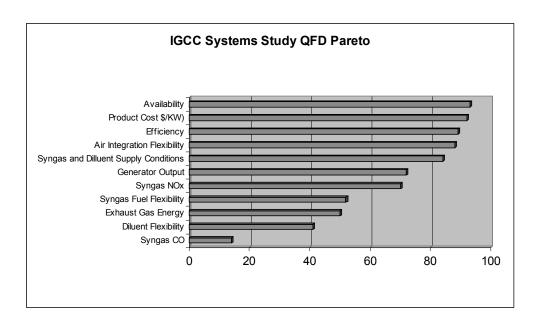


Figure 2 – Pareto for Plant Level QFD

The following 7 IGCC Gas Turbine System Level Parameters were selected as the most significant for further analysis of IGCC system requirements at the power island level:

- 1) Availability
- 2) Product Cost
- 3) Efficiency
- 4) Air Integration Flexibility
- 5) Syngas and Diluent Supply Conditions
- 6) Generator Output
- 7) Syngas NO_x Capability

Task 2 Status/Discussion:

Overview: Gas turbine cycle requirements were identified, analyzed and prioritized relative to achieving plant level goals, and compared with the flowdown of power island goals through use of a Six Sigma Quality Functional Deployment (QFD) Tool.

Task 2 Discussion:

The previous Plant Level Requirements are flowed down as part of the QFD process to yield the following set of Power Island Level Expectations (with corresponding levels of Importance):

Y's

Gas Turbine Power Island Requirements	Importance
Availability	5
Gas Turbine Cost (\$/KW)	5
Efficiency	5
Air Integration Flexibility	5
Syngas and Diluent Supply Conditions	5
Exhaust NO _x	4
Generator Output	4
Syngas Fuel Flexibility	3
Exhaust Gas Energy	3
Diluent Flexibility	3
Exhaust CO	2

A corresponding set of Gas Turbine Cycle Requirements were established as input to the Quality Functional Deployment analysis:

X's

Gas Turbine Cycle Design Options	Notes:
Compressor Air Flow	Impacts size and cost
Compressor Pressure Ratio	Impacts GT plant efficiency, output
Firing Temperature	Maximize for HGP materials
Combustor Pressure Drop	Minimize
Cooling Flows	Minimize
Syngas Supply Temperature	Maximize
Syngas Supply Pressure	Minimize
Diluent Supply Temperature	Maximize
Diluent Supply Pressure	Minimize
Diluent Flow	Optimize
Diluent Type	Nitrogen, Steam, Pre-Moisturized
Turbine & Compressor Efficiency	Optimize for syngas fuel
Combustor Options	Diffusion, Premix Combustors
Percent Air Extraction	Air Extraction Range, Effects on Performance
Exhaust Temperature	Gas Turbine Exhaust Effects

These Gas Turbine Cycle Design options and Power Island Requirements are mapped through the Six Sigma QFD tool, with the weighting factors for the expectations, and the Y's are analyzed against the X's through Low, Medium and High levels of connection, with the following results matrix as shown in Figure 3:

IGCC System Gas Turbine

	Ga	as	Tu	rbii	ne	Tra	ade	ott	t R	eqı	Jire	me	ent	S				
Gas Turbine Power Island Requirements	Importance	Firing Temperature	Combustor Options - NOx Range	Turbine & Compressor Efficiency	Compressor Pressure Ratio	Cooling Flows	Percent Air Extraction	Syngas Supply Temperature	Diluent Supply Temperature	Compressor Air Flow	Diluent Flow	Diluent Type	Combustor Pressure Drop	Syngas Supply Pressure	Diluent Supply Pressure	Exhaust Temperature		Total
Air Integration Flexibility	5	L	М	М	Н	L	Н		L	M			L		L	L		165
Availability	5	Н	М			Н	М											120
Efficiency	5	Н	М	М	Н	Н	М	М	М	L	M	М	М			М		275
Gas Turbine Cost \$/KW)	5	Н	М	Н	М	L	L	М	М	М	L	L	L	L	L	L		205
Syngas and Dilluent Supply Conditions	5		Н	М	Н		М	Н	Η		М	М	М	Н	Н			345
Generator Output	4	Н	М	Н	L	М	М	L	L	Н	М	М	L			М		196
Syngas NOx	4	Н	H	Η:	L	М	M	М	M		М	L	M				_	188
Diluent Flexibility	3		Н	Η:	ļ.,		Ļ		L		M	М	L		L	M	_	93
Exhaust Gas Energy	3	Η.	M	H	Н	М	<u> </u>			М		L	.			М	_	126
Syngas Fuel Flexibility	3	M	Н	M		N #	L	М	H		L	H	L	M			\dashv	69
Syngas CO	2	IVI	Н	М	l	М	М	L	L		L	L	L				\dashv	52
Total		248	234	231	185	139	134	102	101	80	76	68	64	59	58	55		

Figure 3 – Matrix for IGCC Gas Turbine QFD

An alternate representation of the results of the QFD process is the Pareto Chart in Figure 4:

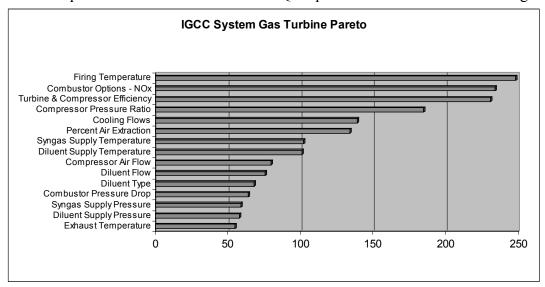


Figure 4 – Pareto for Gas Turbine QFD

The following 11 IGCC Gas Turbine Parameters were selected as the most significant for analysis of Baseline and other IGCC system configurations:

- 1) Firing Temperature
- 2) Combustor Options
- 3) Turbine Efficiency
- 4) Compressor Efficiency
- 5) Compressor Pressure Ratio
- 6) Cooling Flows
- 7) Percent Air Extraction
- 8) Syngas Supply Temperature
- 9) Diluent Supply Temperature
- 10) Compressor Air Flow
- 11) Diluent Flow

Task 3 - Status/Discussion:

Overview: A Baseline IGCC Plant configuration and its performance design basis were chosen. An integrated simulation analysis model of IGCC was constructed to validate the Baseline IGCC Plant model against published performance data. The model was exercised by a parametric analysis to quantify the influence of key gas turbine parameters on performance impact at the IGCC plant system level. Various gas turbine cycle design options were chosen to evaluate performance effects on IGCC at plant level and select appropriate gas turbine technical improvements.

Task 3 Discussion:

Task 3.1 – Establish IGCC System Design Basis

During this task, a Baseline IGCC System was chosen as follows:

- 1) Determined the appropriate gasifier and F-Class Baseline IGCC Plant configuration.
- 2) Evaluated the Energy Flow "Sankey Diagram" for the Baseline IGCC Plant.
- 3) Evaluated overall heat and mass balances for Baseline IGCC Plant.
- 4) Developed an Integrated IGCC Simulation Analysis Model for the Baseline IGCC Plant configuration, and validated this model against published performance data.

The Reference Plant was chosen on the basis of a design which was representative of GE Frame 7FA+e current technology with sufficient public information to perform a detailed performance comparison with the results for that configuration by the Integrated IGCC Simulation Analysis Model. The chosen plant design was the Nordic Energy of Ashtabula (1) case with:

- ISO ambient conditions
- Pittsburgh No. 8 Coal
- Oxvgen blown gasifier
- High pressure cryogenic Air Separation Unit

- HP steam heat recovery similar to Ashtabula study
- COS hydrolysis, wet particulate removal
- Syngas saturation, heating and low temperature heat recovery
- Amine based acid gas cleanup and sulfur recovery
- 7FA+e gas turbine with 2300 °F firing temperature
- Air extraction and N₂ injection
- 3 pressure HRSG
- Reheat 1450 psig/1000F/1000F/ 1.5 in. steam turbine
- Cooling tower, transformer and plant auxiliaries included

The overall configuration of the Baseline Plant is given in Figure 5:

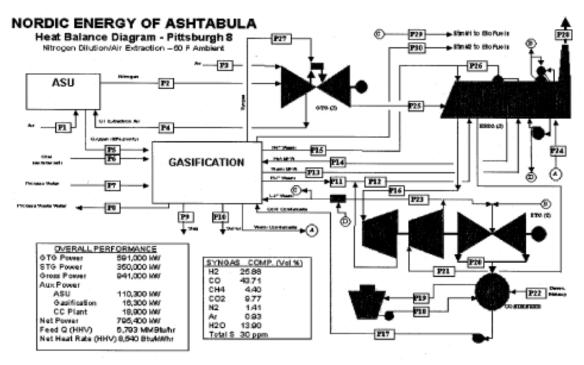


Figure 5 – Baseline IGCC Plant Configuration and Performance

Task 3.2 – Develop System Models and Analyze IGCC System Performance

An Integrated IGCC Simulation Analysis Model for the Baseline IGCC Plant configuration was developed with the following configuration and capabilities:

- Oxygen blown gasifier
- Air extraction integrated high pressure Air Separation Unit
- Gas turbine cycle for detailed performance evaluation
- 3 pressure, reheat steam cycle
- N₂ saturation and injection
- Syngas fuel saturation and heating
- Syngas heat recovery
- Sulfur removal and recovery

This Simulation Analysis Model as shown in Figure 6 utilized in-house tools including a GateCycleTM model of a gas turbine suitable for syngas fuel application. This gas turbine model was integrated with a steam turbine, HRSG combined cycle model using GateCycleTM software. This combined cycle subsystem model was integrated, through use of ModelCenter commercial Software, with a performance simulation model of gasification, ASU, syngas cooling and AGR subsystems utilizing HYSIS commercial software.

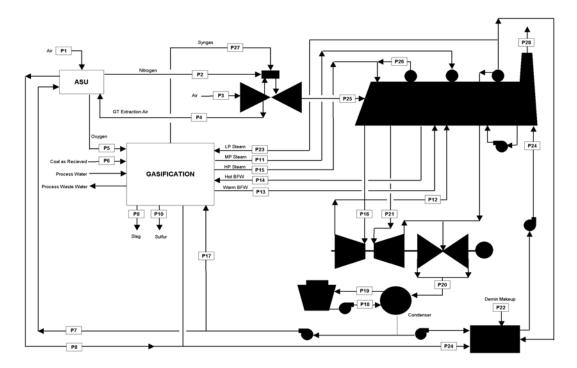


Figure 6 - Integrated IGCC Simulation Analysis Model of Baseline IGCC Plant

The Simulation Analysis Model of the Baseline Case yielded results in very good agreement with the published literature of Nordic Energy Ashtabula Plant. A comparison of syngas compositions for the model and simulation cases in Table 2 shows very good agreement (with Simulation results scaled up to be consistent with the 3x7FA+e Ashtabula and 2x7FA+e Baseline Case configurations).

Table 2 - Syngas Composition Comparison of published data and Simulation Model

Syngas Compositions (Mole Percent)

Species	Nordic Energy Ashtabula Case	Simulation Case
H_2	25.88	25.99
CO	43.71	43.94
$\mathrm{CH_4}$	4.40	4.42
CO_2	9.77	9.67
N_2	1.41	1.09
Ar	0.93	1.06
H_2O	13.90	13.83

A comparison of performance data for the Ashtabula and Simulation case in Table 3 also showed very good agreement. We note that the Baseline Case simulation exhibits an appreciably better heat rate since the Baseline Case simulation does not contain the modest co-generation steam included in the Ashtabula case)

Table 3 – Comparison of Plant Performance for Model and Simulation Cases

IGCC Plant Performance

Parameter	Nordic Energy Ashtabula Case	Simulation Case
Gas Turbine Output (MW)	591.0	590.7
Steam Turbine Output (MW)	350.0	343.5
Auxiliary Power (MW)	-145.5	-141.5
Net Power Output (MW)	795.4	792.7
- , ,		
Net Heat Rate (HHV) (Btu/Kw	-hr) 8540.	8464.

The Baseline IGCC configuration was further modified to model a 207FA+e based IGCC plant and incorporated the following additional changes:

- 1) Air extraction heat recovery
- 2) GE steam turbine with suitable LP last stage

The syngas composition, summary performance and streams data for the Modified Baseline Case are presented in Tables 4, 5 and 6 respectively.

Table 4 – Syngas Composition for Modified Baseline Case

Syngas Comp	Vol %
H2	25.97%
CO	43.89%
CH4	4.42%
CO2	9.66%
N2	1.09%
Ar	1.06%
H2O	13.90%
Total S	31.2 ppm

Table 5: Modified Baseline 207 FA +e IGCC Summary Performance

Overall Performance		<u>Units</u>
GT Power	393200	kW
ST Power	227600	kW
Aux Power		
ASU	71800	kW
Gasification	11400	kW
CC Plant	11100	kW
Net Power	526500	kW
Feed Q (HHV)	4429	MMbtu/hr
Net Heat Rate (HHV)	8413	Btu/kW-hr
Net Efficiency (HHV)	40.59%	
Net Heat Rate (LHV)	8126	Btu/kW-hr
Net Efficiency (LHV)	42.03%	

Table 6: Major Streams Data of Modified Baseline IGCC

<u>Stream</u>	<u>Description</u>	Flow (lb/hr)	Pressure (psia)	Temperature (F)
P1	Air to ASU	812700	14.7	59
P2	Nitrogen to GT	961700	340	533
P3	Air to GT	6667600	14.7	59
P4	Air Extraction from GT	466700	234	771
P5	O2 to Gasification	289100	624	240
P6	Coal (as received)	334000		
P7	Cond to ASU	372100	35	88
P8	Cond Return from ASU	372100	32	221
P9	Slag	52400		
P10	Sulfur	7100		
P11	MP steam from Gasification	16200	423	455
P12	Cold Reheat Steam	1076900	394	654
P13	MP BFW	16200	426	407
P14	Hot BFW	609500	1746	561
P15	HP Steam	609500	1746	617
P16	Superheated HP Steam	1099500	1682	1034
P17	Cold Condensate	1006700	80	88
P18	Cond CW Supply	84824800		71
P19	Cond CW Return	84824800		86
P20	Steam Turbine Exhaust	1270800	0.7367	92
P21	Hot Reheat Steam	1301100	371	1034
P22	Demin Makeup	220000	15	59
P23	LP steam Extraction	75900	70	607
P24	Warm Condensate	876200	159	174
P25	GT Exhaust	7934100	17	1079
P26	HRSG HP Steam	490000	1731	616
P27	Syngas	745500	375	533
P28	HRSG Stack	7934100	15	268
P29	Steam Injection to GT	0	388	653

Task 3.3 – Develop Gas Turbine Conceptual Design Options

Gas turbine cycle design options illustrated in Figure 7 were developed by varying the selected system parameters such as Air Integration Method, ASU type, Diluent Method, and Fuel Temperature, as well as gas turbine parameters such as Combustor Type, Hot Gas Path Configuration, Firing Temperature and Target NO_x Level.

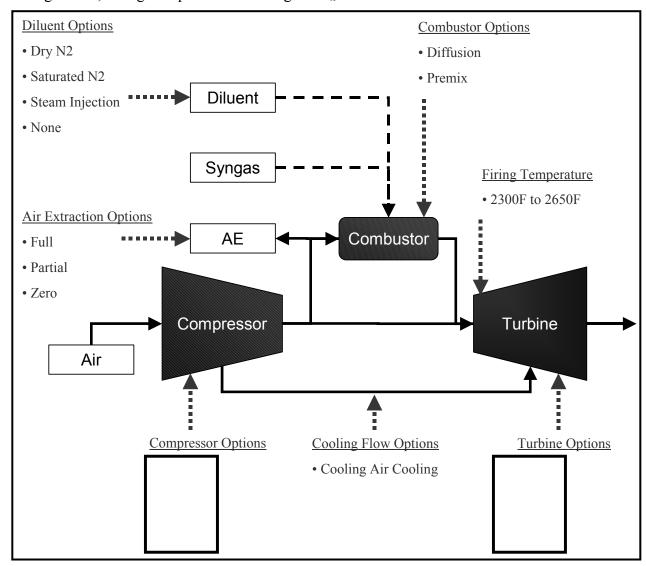


Figure 7 - Gas Turbine Configuration Options

IGCC subsystem models developed in the previous task were exercised to create performance results for these cycle configurations in the integrated IGGC environment. These configuration performance results enable the determination of the performance effects of gas turbine technical improvements on IGCC plant-level performance.

Configuration details for the Base Case and 18 chosen Conceptual Design Options are presented in the following Tables 7 through 10:

Table 7 – Conceptual Design Option Results for Base Case and Cases 1 – 4.

	Gas Turbine	and System	s Configura	tions	
<u>Parameters</u>	<u>Base</u>	<u>Case 01</u>	<u>Case 02</u>	<u>Case 03</u>	<u>Case 04</u>
ASU Type	EP	EP	EP	EP	LP
Air Integration	Partial	Partial	Partial	Full	None
Diluent Type	N2 + Fuel Sat	N2 Sat + Fuel Sat	N2 Sat + Fuel Sat	N2 Sat + Fuel Sat	Steam Inj + Fuel Sat
Fuel Temperature	533	533	533	533	533
Compressor					
Combustor Type	Diffusion	Diffusion	Diffusion	Diffusion	Diffusion
Cooling Air Cooling	No	No	No	No	No
HGP Type					
Stage 1					
Stage 2					
Stage 3					
SCR	None	None	Yes	Yes	Yes
GT Target Output (MW)					
Firing Temperature (F)	2300	2400	2500	2500	2500
NOx (ppmvd @ 15%O2)	15	15	9	9	9

These Conceptual Design Options were set up to cover the gamut of turbine options within the available, as well as future, hardware components. First three cases use diffusion combustion, FB compressor and variation of turbine hot gas path geometry. Case 1 does not use SCR and limits NOx emissions to current EPA emission standards at 15 ppmvd @15% corrected O2. Case 2 and 3 use SCR to get single digit NOx. Cases 4 and 5 use no air integration, standard low pressure cryogenic ASU, fuel saturation, current Natural gas fueled FB gas turbine Hot Gas Path and scaled down FB compressor. Case 4 uses Diffusion combustor and SCR, while Case 5 uses Premix combustor to limit NOx to 15 ppmvd@15% corrected O2.

Table 8 – Conceptual Design Option Results for Cases 5 – 9

	Gas Turbine	and System	ns Configura	tions	
<u>Parameters</u>	<u>Case 05</u>	<u>Case 06</u>	<u>Case 07</u>	<u>Case 08</u>	<u>Case 09</u>
ASU Type	LP	EP	EP	EP	EP
Air Integration	None	Partial	None	Full	Full
Diluent Type	Fuel Sat	N2 Sat + Fuel Sat	N2 Inj + Fuel Sat	N2 Inj	N2 Sat + Fuel Sat
Fuel Temperature	533	533	533	750	533
Compressor					
Combustor Type	DLN	DLN	DLN	DLN	Diffusion
Cooling Air Cooling	No	No	No	No	No
HGP Type					
Stage 1					
Stage 2					
Stage 3					
SCR	Yes	None	None	Yes	None
GT Target Output (MW)					
Firing Temperature (F)	2500	2500	2500	2550	2400
NOx (ppmvd @ 15%O2)	9	9	9	9	15

Table 9 – Conceptual Design Option Results for Cases 10 – 14

	Gas Turbine	and System	ns Configura	tions	
<u>Parameters</u>	<u>Case 10</u>	<u>Case 11</u>	<u>Case 12</u>	<u>Case 13</u>	Case 14
ASU Type	EP	LP	EP	EP	EP
Air Integration	None	None	Partial	Full	Partial, 50%
Diluent Type	N2 Inj + Fuel Sat	Fuel Sat	N2 Sat + Fuel Sat	N2 Sat + Fuel Sat	N2 Sat + Fuel Sat
Fuel Temperature	533	533	600	600	600
Compressor					
Combustor Type	Diffusion	DLN	DLN	DLN	DLN
Cooling Air Cooling	No	No	No	No	No
HGP Type					
Stage 1					
Stage 2					
Stage 3					
SCR	None	None	None	None	None
GT Target Output (MW)					
Firing Temperature (F)	2400	2400	2550	2550	2600
NOx (ppmvd @ 15%O2)	15	15	9	9	9

Cases 6 through 9 use Elevated Pressure ASU, Premix combustor, standard FB compressor and variation of turbine hot gas path geometry. Cases 6 and 7 use enough diluent as not to require SCR, while Case 8 requires SCR to limit NOx to single digit level. Cases 9 through 11 use FA+e compressor and turbine hot gas path geometry and no SCR to limit NOx to 15 ppmvd@15% corrected O2. Case 9 and 10 use Diffusion combustor, EP ASU and N2 and fuel saturation as diluents. Case 11 uses LP ASU and saturated fuel in a premix combustor. Cases 12 through 16 use new compressor and turbine geometry, premix combustor and higher fuel and diluent temperatures to increase thermal efficiency. Cases 12 through 14, use nitrogen and fuel saturation but no SCR, while Cases 15 and 16 use SCR to limit NOx to single digits.

Table 10 – Conceptual Design Option Results for Cases 15 – 18

	Gas Turbine	and System	ns Configura	tions
<u>Parameters</u>	<u>Case 15</u>	<u>Case 16</u>	<u>Case 17</u>	<u>Case 18</u>
ASU Type	EP	EP	EP	EP
Air Integration	Partial, 50%	Full	Partial	Partial
Diluent Type	N2 + Fuel Sat	N2 Sat + Fuel Sat	N2 Sat + Fuel Sat	N2 Sat + Fuel Sat
Fuel Temperature	600	600	533	533
Compressor				
Combustor Type	DLN	DLN	Diffusion	Diffusion
Cooling Air Cooling	Yes	No	Yes	No
HGP Type				
Stage 1				
Stage 2				
Stage 3				
SCR	Yes	Yes	None	None
GT Target Output (MW)				
Firing Temperature (F)	2600	2650	2400	2500
NOx (ppmvd @ 15%O2)	9	9	2	2

Cases 14 through 16 use higher firing temperature than current FB and reduced cooling by utilizing new CMC materials for turbine first stage nozzles. Case 15 even explores the potential of using external turbine cooling air. Cases 17 and 18 explore Diffusion combustor and new turbine hot gas path design to reach DOE goals of 2 ppm NOx limit without SCR by increasing diluent flow to the limit by saturation of N2 and fuel.

The 18 options represent reasonable, compatible options, which explore the region of attractive turbine configurations with aim to provide improved performance, increased output, efficiency and reduced NOx emissions for IGCC systems.

Task 4 - Status/Discussion:

Overview: The integrated IGCC system analysis model developed in Task 3 was used to determine the influence coefficients of vital gas turbine parameters (firing temperature, turbine and compressor efficiency, compressor pressure ratio, cooling flow, fuel and diluent temperature, etc.) on key plant-level performance goals (net plant efficiency, net output, NOx emissions, etc.). The analysis model was utilized to perform IGCC performance trade-off analysis of various gas turbine cycle design options in order to determine which options best meet DOE IGCC Plant Goals

Task 4 Discussion:

Task 4.1: - Determine Gas Turbine Vital Parameters Influence on Plant Level Performance IGCC simulation model was exercised to determine the influence coefficients on four key IGCC plant level performance parameters namely, net efficiency, net output, gas turbine output and NOx emissions of the 11 selected gas turbine cycle parameters.

Influence coefficients, as shown in Table 11, are defined as the relative change in IGCC plant performance parameter such as IGCC net efficiency for an incremental change in gas turbine cycle parameter, such as Firing temperature or relative slope value, (DY/Y) /(DX/X), where X and Y refer to values for Baseline IGCC system.

Table 11: Gas Turbine Cycle Influence Coefficients on IGCC Performance

Turbine Cycle Parameter	IGCC Net Eff	IGCC Net kW	GT Output	NOx
Firing Temperature	0.584	3.113	2.948	2.604
Turbine Isen Efficiency %	0.784	0.784	2.070	0.000
Compressor Isen Efficiency %	0.252	0.669	0.937	0.130
Compressor Air Flow	-0.026	0.970	1.007	0.000
Compressor Pressure Ratio	-0.048	-0.361	-0.144	0.910
Turbine Cooling Flow	-0.045	-0.180	-0.208	0.525
Combustor DP/P	-0.010	-0.009	-0.026	0.207
Nitrogen Dilluent Flow	0.020	0.192	0.294	-3.869
Diluent Supply Temperature	0.063	-0.055	-0.058	0.715
Syngas Supply Temperature	0.030	-0.110	-0.078	0.840
Air Extraction	-0.003	-0.087	-0.154	0.044

Results show that gas turbine Firing Temperature, Turbine & Compressor Efficiency, Diluent Supply Temperature, Compressor Pressure Ratio and Cooling Flows have the maximum impact on IGCC net efficiency.

IGCC net output was most impacted by Firing Temperature, Compressor Inlet Air Flow, Turbine & Compressor Efficiency, Compressor Pressure Ratio and Dilution Flow respectively.

Gas Turbine Output was most impacted by Firing Temperature, Turbine & Compressor Efficiency and Compressor Inlet Air respectively.

Combustion Technology (Diffusion or Premix), Diluent flow, Firing Temperature and Compressor Pressure Ratio have the most impact on NOx Emissions.

The analysis results indicate that IGCC performance is most influenced by gas turbine internal design parameters such as Firing Temperature, Turbine and Compressor geometry, Combustion and Cooling technology. IGCC cycle integration parameters such as Fuel and Diluent Flow and supply conditions have secondary impact except for NOx emissions.

Task 4.2: - Perform Design Trade-off Analysis

Eighteen new gas turbine cycle designs were selected in Task 3.3 for conducting IGCC plant performance trade-off studies. These studies utilized IGCC System Performance Simulation Model developed in task 3.2. Tables 12 through 17 show IGCC summary performance and major streams data of these cases. Results indicate that IGCC efficiency gains up to 2.8 pts, from 40.5% to 43.3% and IGCC net output gains up to 25 % are possible due to improvements in gas turbine technology alone with single digit NOx emission levels.

Table 12: IGCC Summary Performance of Gas Turbine Cycle Design Cases 1 thru 6

	<u>Units</u>	<u>Case 01</u>	<u>Case 02</u>	<u>Case 03</u>	<u>Case 04</u>	<u>Case 05</u>	<u>Case 06</u>
GT Power	kW						
ST Power	kW						
Aux Power	ľ						
ASU	kW	100400	81700	33700	54300	48900	81700
Gasification	kW	14500	13500	11500	11900	11300	13500
CC Plant	kW	12200	12500	11000	9700	10700	12500
Net Power	kW	623000	652100	544300	548100	537800	652400
Feed Q (HHV)	MMbtu/hr	5080	5212	4424	4587	4347	5213
Net Heat Rate (HHV)	Btu/kW-hr	8154	7993	8127	8369	8083	7990
Net Efficiency (HHV)		41.88%	42.73%	42.02%	40.81%	42.25%	42.74%
Net Heat Rate (LHV)	Btu/kW-hr	7876	7721	7850	8084	7808	7718
Net Efficiency (LHV)		43.36%	44.23%	43.51%	42.25%	43.74%	44.25%
GT Parameters	<u>Units</u>						
Combustor Type		Diffusion	Diffusion	Diffusion	Diffusion	Premix	Premix
CPR	j						
Tfire	F	2400	2500	2500	2500	2500	2500
Texh	F						
Stack NOx	ppmvd@15% O2	15	9	15	9	9	9
GT Spec Output	kW-s/lb	254.4	255.0	189.0	263.5	209.9	255.2
IGCC Spec Output	kW-s/lb	165.3	173.0	144.4	171.3	151.6	173.1
CC LHV % Eff Exh Dp	in H2O	65.8% -15.0	65.0% -15.9	60.5% -15.9	60.7% -16.1	62.4% -16.1	65.1% -15.0

Table 13: IGCC Summary Performance of Gas Turbine Cycle Design Cases 7 thru 12

Description	<u>Units</u>	<u>Case 07</u>	<u>Case 08</u>	<u>Case 09</u>	<u>Case 10</u>	<u>Case 11</u>	<u>Case 12</u>
GT Power	kW						
ST Power	kW						
Aux Power							
ASU	kW	122300	30200	40900	96200	49400	79800
Gasification	kW	15000	11500	11400	11700	11400	13300
CC Plant	kW	13600	11100	11000	10900	10800	12200
Net Power	kW	724600	552700	535300	546600	539600	647600
Feed Q (HHV)	MMbtu/hr	5782	4437	4388	4501	4396	5140
Net Heat Rate (HHV)	Btu/kW-hr	7980	8027	8197	8235	8147	7936
Net Efficiency (HHV)		42.80%	42.55%	41.66%	41.47%	41.92%	43.03%
Net Heat Rate (LHV)	Btu/kW-hr	7708	7754	7918	7954	7870	7666
Net Efficiency (LHV)		44.31%	44.05%	43.13%	42.93%	43.40%	44.55%
GT Parameters	<u>Units</u>						
Combustor Type		Premix	Premix	Diffusion	Diffusion	Premix	Premix
CPR							
Tfire	F	2500	2550	2400	2400	2400	2550
Texh	F						
Stack NOx	ppmvd@15% O2	9	9	15	15	15	9
GT Spec Output	kW-s/lb	303.0	191.5	189.9	266.0	198.5	255.0
IGCC Spec Output	kW-s/lb	192.3	146.7	142.0	170.2	143.2	171.8
CC LHV % Eff Exh Dp	in H2O	67.6% -15.0	60.8% -16.1	60.7% -15.0	65.9% -15.0	61.9% -15.0	65.4% -15.0

Table 14: IGCC Summary Performance of Gas Turbine Cycle Design Cases 13 thru 18

Description	<u>Units</u>	<u>Case 13</u>	<u>Case 14</u>	<u>Case 15</u>	<u>Case 16</u>	<u>Case 17</u>	<u>Case 18</u>
GT Power	kW						
ST Power	kW						
Aux Power							
ASU	kW	55500	86100	83000	50700	78700	74700
Gasification	kW	14300	13900	13600	12800	13500	12700
CC Plant	kW	13200	12600	12700	12000	10700	10100
Net Power	kW	694700	672200	664200	624500	625800	594400
Feed Q (HHV)	MMbtu/hr	5537	5352	5239	4930	5213	4883
Net Heat Rate (HHV)	Btu/kW-hr	7970	7962	7888	7894	8329	8215
Net Efficiency (HHV)		42.85%	42.89%	43.29%	43.26%	41.00%	41.57%
Net Heat Rate (LHV)	Btu/kW-hr	7698	7691	7620	7625	8046	7935
Net Efficiency (LHV)		44.36%	44.41%	44.82%	44.79%	42.45%	43.04%
GT Parameters	<u>Units</u>						
Combustor Type		Premix	Premix	Premix	Premix	Diffusion	Diffusion
CPR							
Tfire	F	2550	2600	2600	2650	2400	2500
Texh	F						
Stack NOx	ppmvd@15% O2	9	9	9	9	2	2
GT Spec Output	kW-s/lb	215.0	267.8	260.9	229.4	300.3	329.1
IGCC Spec Output	kW-s/lb	155.3	178.4	176.2	165.7	186.5	203.8
CC LHV % Eff		62.7%	65.6%	66.0%	63.4%	62.4%	63.3%
Exh Dp	in H2O	-15.0	-15.0	-16.1	-16.1	-15.0	-15.0

Table 15a: IGCC Major Streams Data of Gas Turbine Cycle Design Cases 1 thru 6

Stream	Description	<u>Units</u>	<u>Case 01</u>	Case 02	<u>Case 03</u>	Case 04	<u>Case 05</u>	(
21	Air to ASU							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
2	Diluent to GTs							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
	Ar	Mol %						
	CO2	Mol %						
	H2O							
		Mol %						
	N2	Mol %						
	02	Mol %						
23	Air to GTs							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
4	Air Extraction from 0							
•	Flow	lb/hr	II					
	Pressure							
		psia	II					
	Temperature	F						
25	O2 to Gasification							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
96	Coal (as received)							
	Flow	lb/hr						
7	Cond to ASU							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
28								
8	Cond Return from A							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
9	Slag							
	Flow	lb/hr						
210	Sulfur		II					
	Flow	lb/hr						
11	MP steam from Gasi							
	Flow	lb/hr	II					
	Pressure	psia	II					
	Temperature	F						
212	Cold Reheat Steam	'						
12		lh/hr						
	Flow	lb/hr						
	Pressure	psia	II					
	Temperature	F	II					
13	MP BFW							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
214	Hot BFW							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F	II					
P15	HP Steam	'						
13	Flow	lh/h=	II					
		lb/hr						
	Pressure	psia						
	Temperature	F	III					

Table 15b: IGCC Major Streams Data of Gas Turbine Cycle Design Cases 1 thru 6 (Cont')

Stream	Description	<u>Units</u>	<u>Case 01</u>	<u>Case 02</u>	<u>Case 03</u>	<u>Case 04</u>	<u>Case 05</u>	Case
P16	Superheated HP Stean							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P17	Cold Condensate							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P18		г						
P10	Cond CW Supply							
	Flow	lb/hr						
	Temperature	F						
P19	Cond CW Return							
	Flow	lb/hr						
	Temperature	F						
P20	Steam Turbine Exhaus							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P21	Hot Reheat Steam							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P22	Demin Makeup							
	Flow	lb/hr						
	Pressure	psia						
P23	Temperature	F						
P23	LP steam Extraction Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P24	Warm Condensate	'						
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P25	GT Exhaust (per GT)	·						
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P26	HRSG HP Steam							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P27	Syngas (per GT)							
	Flow	lb/hr						
Fuel/Dil Ra								
	Pressure	psia F						
	Temperature							
	H2 CO	Mol % Mol %						
	CH4	Mol %						
	CH4 CO2	Mol %						
	N2	Mol %						
	Ar	Mol %						
	H2O	Mol %						
	Total S	ppm						
P28	HRSG Stack	ppin						
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P29	Steam Injection to GT							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						

Table 16a: IGCC Major Streams Data of Gas Turbine Cycle Design Cases 7 thru 12

Air to ASU Flow Ibhr Pressure pails Temperature F				0 07	0 00	0 00	0 10	0 44	
Flow bhr Pressure paia Temperature F Diluent to GTs Flow bhr Pressure paia Temperature F Ar Mol % CO2 Mol % H2O Mol % N2 Mol % Alt to GTs Flow bhr Pressure paia Temperature F Ar Extraction from GTs Flow lbhr Pressure paia Temperature F Ar Extraction from GTs Flow lbhr Pressure paia Temperature F Co desification Flow lbhr Pressure paia Temperature F Cond to ASU Flow lbhr Pressure paia Temperature F Cond to ASU Flow lbhr Pressure paia Temperature F Cond to ASU Flow lbhr Pressure paia Temperature F Cond Return from ASU Flow lbhr Pressure paia Temperature F Cond Return from ASU Flow lbhr Pressure paia Temperature F Cond Return from ASU Flow lbhr Pressure paia Temperature F Cond Return from Gasification Flow lbhr Pressure paia Temperature F Cold Retard Stam Flow lbhr Pressure paia Temperature F HP Stew Flow lbhr Pressure paia Temperature F HO BFW Flow lbhr Pressure paia Temperature F HO BEW Flow lbhr Pressure paia	<u>Stream</u>	<u>Description</u>	<u>Units</u>	<u>Case 07</u>	<u>Case 08</u>	<u>Case 09</u>	<u>Case 10</u>	<u>Case 11</u>	<u>C</u>
Pressure paia Temperature F Diluent to GTs Flow	21								
Temperature F				ll .					
Diluent to GTs				ll .					
Flow		Temperature	F	ll .					
Flow	2	Diluent to GTs		ll .					
Pressure			lb/hr	ll .					
Temperature				ll .					
Ar Mol % H2O Mol % H2O Mol % Q2 Mol % Air to GTs Flow Ibhr Pressure psia Temperature F Air Extraction from GTs Flow Ibhr Pressure psia Temperature F Q2 to Gastification Flow Ibhr Pressure psia Temperature F Coal (as received) Flow Ibhr Pressure psia Temperature F Cond to ASU Flow Ibhr Pressure psia Temperature F Cond Return from ASU Flow Ibhr Pressure psia Temperature F Coal Remarks F Coal Remarks F F F F F F F F F F F F F				ll .					
CO2 Mol % N2 Mol % Q2 Mol % Air to GTs Flow Ibhr Pressure psia Temperature F Air Extraction from GTs Flow Ibhr Pressure psia Temperature F Ocal (as received) Flow Ibhr Pressure psia Temperature F Coal (as received) Flow Ibhr Pressure psia Temperature F Coal (as received) Flow Ibhr Pressure psia Temperature F Siag Temperature F Cond Return from ASU Flow Ibhr Pressure psia Temperature F Cond Return from ASU Flow Ibhr Pressure psia Temperature F Cond Return from Gasification Flow Ibhr Pressure psia Temperature F Cod Return from Gasification Flow Ibhr Pressure psia Temperature F Siag Flow Ibhr Pressure psia Temperature F Cod Return from Gasification Flow Ibhr Pressure psia Temperature F Cod Return from Gasification Flow Ibhr Pressure psia Temperature F Cod Return from Gasification Flow Ibhr Pressure psia Temperature F N P BFW Flow Ibhr Pressure psia Temperature F HOBEW Flow Ibhr Pressure psia				ll .					
H2O				ll .					
N2 Mol % Air to GTs Flow Ib/hr Pressure psia Temperature F Air Extraction from GTs Flow Ib/hr Pressure psia Temperature F O2 to Gasification Flow Ib/hr Pressure psia Temperature F Coal (as received) Flow Ib/hr Pressure psia Temperature F Coal (as received) Flow Ib/hr Pressure psia Temperature F Cond Return from ASU Flow Ib/hr Pressure psia Temperature F Siag Flow Ib/hr Pressure psia Temperature F Cod Return from ASU Flow Ib/hr Pressure psia Temperature F Cod Return from Gasification Flow Ib/hr Pressure psia Temperature F Siag Flow Ib/hr Pressure psia Temperature F Hot BFW Flow Ib/hr Pressure psia				ll .					
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				II .					
		Temperature	psia F	II .					

Table 16b: IGCC Major Streams Data of Gas Turbine Cycle Design Cases 7 thru 12 (Cont')

		Casa 07	C=== 00	Cana 00	Casa 10	Cana 11	Casa 10
<u>Description</u>	<u>Units</u>	<u>Case 07</u>	<u>Case 08</u>	<u>Case 09</u>	<u>Case 10</u>	<u>Case 11</u>	<u>Case 12</u>
Superheated HP Stear							
Flow	lb/hr						
Pressure	psia						
Temperature	F						
Cold Condensate							
Flow	lb/hr						
Pressure	psia						
Temperature	F						
Cond CW Supply							
Flow	lb/hr						
Temperature	F						
Cond CW Return							
Flow	lb/hr						
Temperature	F						
Steam Turbine Exhau							
Flow	lb/hr						
Pressure	psia						
Temperature	F						
Hot Reheat Steam							
Flow	lb/hr						
Pressure	psia						
Temperature	F						
Demin Makeup							
Flow	lb/hr						
Pressure	psia						
Temperature	F						
LP steam Extraction							
Flow	lb/hr						
Pressure	psia F						
Temperature Warm Condensate	F						
Flow	lb/hr						
Pressure	psia						
Temperature	F						
GT Exhaust (per GT)	•						
Flow	lb/hr						
Pressure	psia						
Temperature	F						
HRSG HP Steam							
Flow	lb/hr						
Pressure	psia						
Temperature	F						
Syngas (per GT)							
Flow	lb/hr						
) 							
Pressure	psia						
Temperature H2	F Mol %						
CO	Mol %						
CH4	Mol %						
CO2	Mol %						
N2	Mol %						
Ar	Mol %						
H2O	Mol %						
Total S	ppm						
HRSG Stack							
Flow	lb/hr						
Pressure	psia						
Temperature	F						
Steam Injection to GT							
Flow	lb/hr						
Pressure	psia						
Temperature	F						

Table 17a: IGCC Major Streams Data of Gas Turbine Cycle Design Cases 13 thru 18

Stream	Description	<u>Units</u>
	Air to ASU	<u> </u>
	Flow	lb/hr
	Pressure	psia
_	Temperature	F
2	Diluent to GTs	
	Flow	lb/hr
	Pressure Temperature	psia F
	Ar	Mol %
	CO2	Mol %
	H2O	Mol %
	N2	Mol %
	O2	Mol %
3	Air to GTs	
	Flow	lb/hr
	Pressure	psia
	Temperature	F
4	Air Extraction from (
	Flow Pressure	lb/hr psia
	Temperature	psia F
5	O2 to Gasification	
	Flow	lb/hr
	Pressure	psia
	Temperature	F
6	Coal (as received)	
	Flow	lb/hr
7	Cond to ASU	
	Flow	lb/hr
	Pressure Temperature	psia F
8	Cond Return from A	
-	Flow	lb/hr
	Pressure	psia
	Temperature	F
9	Slag	
	Flow	lb/hr
10	Sulfur	
	Flow	lb/hr
11	MP steam from Gasi	
	Flow Pressure	lb/hr psia
	Temperature	psia F
12	Cold Reheat Steam	
-	Flow	lb/hr
	Pressure	psia
	Temperature	F
13	MP BFW	
	Flow	lb/hr
	Pressure	psia
4.4	Temperature	F
14	Hot BFW Flow	lb/hr
	Pressure	psia
	Temperature	F
15	HP Steam	
	Flow	lb/hr
	Pressure	psia
	Temperature	F

Table 17b: IGCC Major Streams Data of Gas Turbine Cycle Design Cases 13 thru 18

Stream	<u>Description</u>	<u>Units</u>	<u>Case 13</u>	<u>Case 14</u>	<u>Case 15</u>	<u>Case 16</u>	<u>Case 17</u>	<u>Case 18</u>
P16	Superheated HP Steam	m						
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P17	Cold Condensate	•						
,	Flow	lb/hr						
	Pressure	psia						
		Psia F						
P18	Temperature	Г						
P18	Cond CW Supply	II. II.						
	Flow	lb/hr						
	Temperature	F						
P19	Cond CW Return							
	Flow	lb/hr						
	Temperature	F						
P20	Steam Turbine Exhau							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P21	Hot Reheat Steam	II. II.						
	Flow	lb/hr						
	Pressure	psia F						
P22	Temperature Demin Makeup	г						
PZZ	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P23	LP steam Extraction	•						
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P24	Warm Condensate							
	Flow	lb/hr						
	Pressure	psia						
	Temperature	F						
P25	GT Exhaust (per GT)							
	Flow	lb/hr						
	Pressure	psia						
D00	Temperature	F						
P26	HRSG HP Steam Flow	lb/hr						
	Pressure	psia						
	Temperature	psia F						
P27	Syngas (per GT)							
·	Flow	lb/hr						
Fuel/Dil R	Ratio							
	Pressure	psia						
	Temperature	F						
	H2	Mol %						
	CO	Mol %						
	CH4	Mol %						
	CO2	Mol %						
	N2	Mol %						
	Ar	Mol %						
	H2O	Mol %						
Dae	Total S	ppm						
P28	HRSG Stack Flow	lb/hr						
	Pressure	psia						
	Temperature	psia F						
P29	Steam Injection to GT							
	Flow	lb/hr						466000
	Pressure	psia						
	Temperature	F						

Task 5 - Status/Discussion:

Overview:

Task 5 Discussion: Various GT cycle designs were examined utilizing the performance results to select the most promising candidate cycle concepts. The 3 most promising GT candidates are recommended on the basis of their merit on IGCC Efficiency, IGCC Net Output, GT Specific Output and NOx Emissions. For near term (2006): the recommended GT cycle design should have a 2400F class firing temperature, base class compressor pressure ratio (CPR), diffusion combustor and integrated air extraction; for midterm (2008): a 2500F class firing temperature, base class CPR, diffusion combustor, and integrated air extraction; and for long term (2010): a 2600F class firing temperature, increased CPR, and further combustion and hot gas path technology enhancements. A roadmap of turbine technology development leading to DOE IGCC efficiency goal of 50%, less than \$1000/kw cost and NOx emissions less than 3 ppm is presented.

Task 5 Discussion:

Results of the Trade-Off Analysis utilizing 18 Conceptual Design Options have been used to produce the most promising candidate GT Cycle Design Concepts which best meet DOE goals for this study. The GT Cycle Design Concepts were analyzed relative to Overall IGCC Efficiency, IGCC Specific Power, GT Specific Power, NOx Emissions and shown in Figure 8.

IGCC Plant Performance Vs GT Options

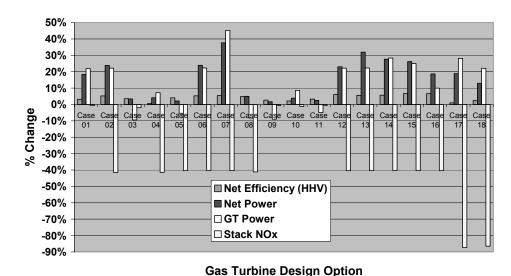


Figure 8: IGCC Plant Performance of GT Design Options

One way to select gas turbine is to analyze the IGCC Efficiency against GT Specific Output as shown in Figure 9 for various GT options. The higher the IGCC efficiency and GT Specific Output, the design option will result in higher cost effective machine.

IGCC Net Efficiency (HHV) Vs GT Specific Output %

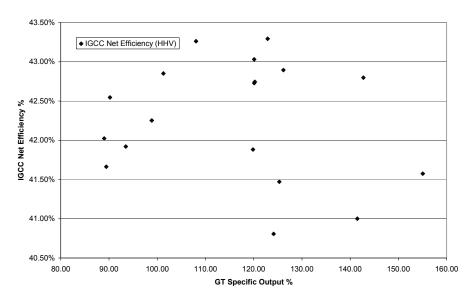


Figure 9: IGCC Net Efficiency vs GT Specific Output for various GT options

Another way to select gas turbine is to analyze the IGCC Specific Output against GT Specific Output as shown in Figure 10 for various GT options. The higher the IGCC specific output and GT Specific Output, the design option will result in higher cost effective machine.

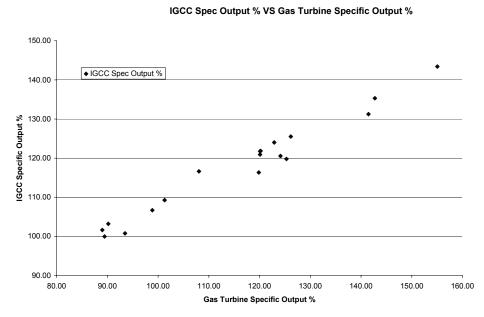


Figure 10: IGCC Specific Output vs GT Specific Output for various GT options

When IGCC Efficiency and IGCC Output have equal importance, the GT options can be selected as the option, which would give both of these higher values as shown in Figure 11.

Optimized IGCC Cycle Selection

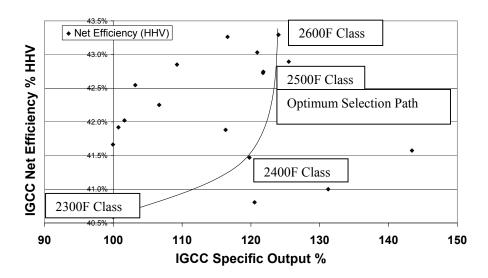


Figure 11: IGCC Net Efficiency vs IGCC Specific Output for various GT options

As GT Cycle Firing temperature increases from 2300F to 2600F, IGCC plant efficiency increases and IGCC Specific Output also increases. An optimum GT cycle selection path is shown in Figure 11, based on increased GT technology development required.

Turbine Technology Development Roadmap: A roadmap of gas turbine technology and development is required to advance beyond today's state-of-the art performance, economics, and emissions for coal based IGCC power plants. Today's IGCC technology delivers 40% efficiency, low double-digit NOx, and competitive COE. Future targets and technologies have been proposed to reach 50% HHV efficiency, with lower capital cost and COE performance, while isolating CO2 and producing less than 3ppm NOx. The recommended technology roadmap is shown in Figure 12.

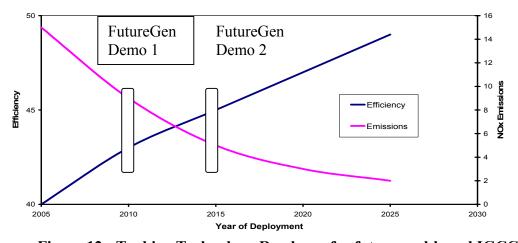


Figure 12: Turbine Technology Roadmap for future coal-based IGCC

Near-Term Developments

Near-term, high efficiency can be accomplished by improving GT cycle technology through conventional means of increased firing temperature and pressure ratio, and through advanced cycle integration concepts. Increased firing temperature, CO2 sequestration, and lower NOx targets all cause additional demands on combustion and turbine technologies related to high-hydrogen combustion and turbine durability. These two challenges are common to the next generations of high technology and very low emissions turbine power plants envisioned by power generation researchers and industry.

High efficiency for the 7FB IGCC will be achieved by performing a system optimization of the integrated cycle, by analyzing the impact of technologies and design choices on performance, reliability, and Cost of Electricity. Further advances in turbine cooling and materials technology will provide significant improvements toward performance and economic objectives: such as allowing increased firing temperature at a given NOx, and reducing turbine cooling flows. Advances are needed in the state-of-art combustor from a diffusion-flame to pre-mix fuel nozzle. improving NOx characteristics on syngas and carbon free high Hydrogen fuels. Current IGCC gas turbine practice involves injection of dilution gas, typically nitrogen or steam, into a diffusion-flame combustor in order to mitigate NOx emissions. As NOx limits are reduced to the 2ppm DOE goal, large amounts of steam will be required for diluent, as nitrogen will not be adequate. Without corresponding combustor improvements, the NOx is most effectively reduced by injecting steam, reducing turbine life by increasing water content and heat transfer. Other methods of improving high H2 combustion performance such as Trapped vortex/ Rich Catalyst/ Exhaust gas Recirculation may also be required to achieve less than 3 ppm NOx emission goals. Ceramic Matrix Composite (CMC) components will provide additional performance advantages in this environment. Not only do CMCs require less cooling than metallic parts in current turbine environments, they will consume less incremental cooling as gaspath heat capacity increases from higher moisture and higher firing temperature.

Long-Term Developments

Long-term coal based IGCC cycles will optimize around improved technologies in all areas of combustion, turbine, air separation unit (ASU), CO2 separation, gasifier, and process island technologies.

There is potential for additional benefit through increased cycle integration using components such as intercoolers, recuperators, and by incorporating novel ideas such as exhaust gas recirculation, reheat combustion, and variable inlet oxygen content. These concepts will present new challenges with regard to risk, costs, startup and transient performance, control and flexibility criteria.

The roadmap shows FutureGen demos in 2010 and 2015. The 2010 configuration would include diffusion-flame combustion with diluent injection and an SCR, using the 7FB optimized for near-term market needs and with the best available injector technologies. The 2015 demo would include features of the advanced combustion systems, with better performance while running on higher hydrogen content. Other aspects of the test would include advanced HGP material and

cooling strategies. The cycle efficiency of these units would demonstrate both progress along the efficiency and emissions roadmap, but also the enabling capabilities required for higher hydrogen turbines proposed for longer-range development.

Conclusions and Recommendations

Conclusions:

Task 1 - Overall IGCC Plant Level Requirements Identification:

Plant level (power island) requirements were identified, and compared with DOE's IGCC Goal of achieving 50% Net HHV Efficiency and \$1000/KW by the Year 2008, through use of a Quality Functional Deployment (QFD) Tool. This analysis resulted in the following 7 Gas Turbine System Level Parameters being selected as the most significant for further analysis of IGCC system Requirements at the power island level:

- 1) Availability
- 2) Product Cost per kW
- 3) Efficiency
- 4) Air Integration Flexibility
- 5) Syngas Supply Conditions
- 6) Diluent Supply Conditions
- 7) Syngas NO_x Capability

Task 2 – Requirements Prioritization & Flow-Down to Gas Turbine Subsystem Level

Gas turbine requirements were identified, analyzed and prioritized relative to achieving plant level goals, and compared with the flowdown of power island goals through use of a Quality Functional Deployment (QFD) Tool. This analysis resulted in the following 11 Gas Turbine Cycle Design Parameters being selected as the most significant for analysis of Baseline and other IGCC system configurations:

- 1) Firing Temperature
- 2) Combustor Options
- 3) Turbine Efficiency
- 4) Compressor Efficiency
- 5) Compressor Pressure Ratio
- 6) Cooling Flows
- 7) Percent Air Extraction
- 8) Syngas Supply Temperature
- 9) Diluent Supply Temperature
- 10) Compressor Air Flow
- 11) Diluent Flow

Task 3 – IGCC Conceptual System Analysis

A Baseline IGCC Plant configuration was chosen, and an integrated IGCC simulation analysis model was constructed to successfully validate the Baseline IGCC Plant Model against published

performance data. The baseline model was optimized by including air extraction heat recovery and GE steam turbine model with appropriate last stage buckets.

Baseline IGCC based on GE 207FA+e gas turbine combined cycle has net HHV efficiency of 40.5% and net output nominally of 526 Megawatts at NOx emission level of 15 ppmvd@15% corrected O2.

Eighteen Advanced F technology gas turbine cycle design options were developed to provide performance targets with increased output and/or efficiency with low NOx emissions for IGCC systems by varying the selected system parameters such as Air Integration Method, ASU type, Diluent Method, and Fuel Temperature, as well as gas turbine parameters such as Combustor Type, Hot Gas Path Configuration, Firing Temperature and Target NO_x Level.

Task 4 – Gas Turbine Cycle Options vs. Requirements Evaluation

Influence coefficients on four key IGCC plant level performance parameters namely, net efficiency, net output, gas turbine output and NOx emissions of the 11 gas turbine cycle parameters were determined. IGCC net efficiency was most impacted by gas turbine Firing temperature, turbine & compressor efficiency, diluent supply temperature, compressor pressure ratio and turbine cooling flows. IGCC net output was most impacted by Firing temperature, compressor inlet air flow, turbine & compressor efficiency, compressor pressure ratio and dilution flow respectively. IGCC Plant NOx emissions were most influenced by gas turbine combustion technology (Diffusion or Premix), Diluent flow, Firing temperature and compressor pressure ratio.

A total of 18 new gas turbine cycle options based on Advanced F technology have been analyzed. Results indicate that IGCC net efficiency HHV gains up to 2.5 pts, from 40.5% to 43.0% and IGCC net output gains up to 25 % are possible due to improvements in gas turbine technology alone with single digit NOx emission levels.

Recommendations

Task 5 – Recommendations for Gas Turbine Technical Improvements

Various GT cycle designs were examined utilizing the performance results to select the most promising candidate cycle concepts. The 3 most promising GT candidates are recommended on the basis of their merit on IGCC Efficiency, IGCC Net Output, GT Specific Output and NOx Emissions. For near term (2006): the recommended GT cycle design should have a 2400F class firing temperature, base class compressor pressure ratio (CPR), diffusion combustor and integrated air extraction; for midterm (2008): a 2500F class firing temperature, base class CPR, diffusion combustor, and integrated air extraction; and for long term (2010): a 2600F class firing temperature, increased CPR, and further combustion and hot gas path technology enhancements.

A Turbine technology roadmap is presented, which will lead to coal based IGCC goals of 50% in efficiency, less than \$1000/kW in cost and NOx emissions less than 3 ppm.

References

1. Integrating Clean Coal Technologies and Cogeneration Opportunities with Industrial Land Reuse", Nordic Energy of Ashtabula LLC, Department of Energy Program Solicitation No. DE-PS26-02NT41428, August 2002.

List of Acronyms and Abbreviations

AGR - Acid Gas Removal sulfur removal sub-system

ASU - Air Separation Unit oxygen plant sub-system

CPR - Compressor Pressure Ratio

EP - **Elevated Pressure Air Separation Unit**

FB - GE's Advanced Air cooled Turbine

GT - **Gas Turbine**

HHV - Fuel Higher Heating Value

HGP - Hot Gas Path

HRSG - Heat Recovery Steam Generator

IGCC - Integrated Gasifier Combined Cycle power plant

LP - Low Pressure Air Separation Unit

NOx - Gaseous mixture of Nitrogen Oxides

SCR - Selective Catalytic Reduction

QFD - Six Sigma Quality Functional Deployment analysis system